



# Integrated Nozzle Flow, Spray and Combustion Modeling Using KH-ACT Primary Breakup Model & Detailed Chemistry

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Argonne National Laboratory

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AEC/HCCI Working Group Meeting at Sandia National Laboratory

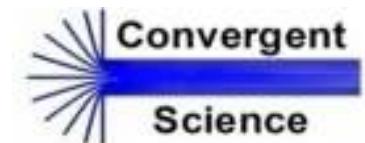


# Collaborators

Ms. Anita I. Ramirez, Prof. Suresh K. Aggarwal at  
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Dr. Peter K. Senecal, Dr. Eric Pomraning at **CONVERGENT Science**



Prof. Tianfeng Lu, Mr. Zhaoyu Luo, Mr. Max Plomer at  
**University of Connecticut**



# Acknowledgements

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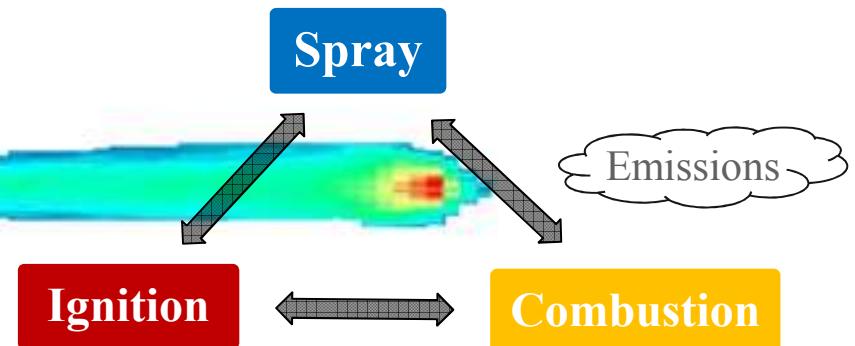
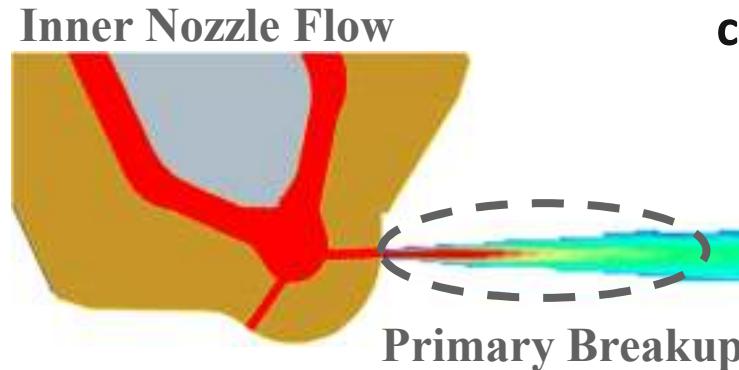
Caterpillar Inc. for hardware and engine support

Dr. Lyle Pickett at Sandia National Laboratory for sharing biodiesel data

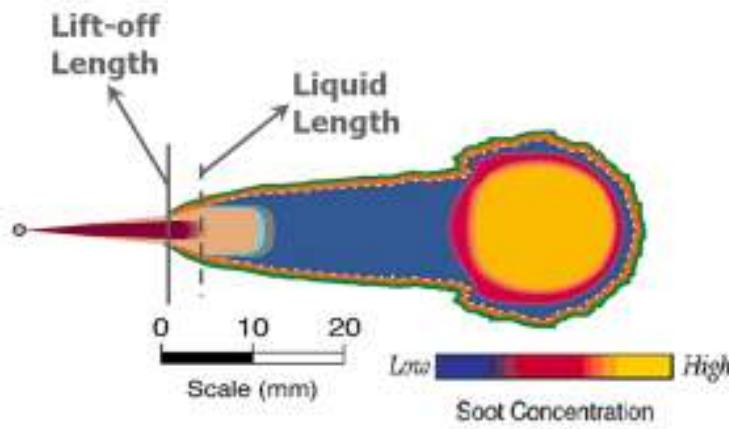


# Integrated Modeling Approach

Influence of fuel properties on nozzle flow, spray, combustion and emission characteristics!!



Conceptual Combustion Model from Sandia National Laboratory



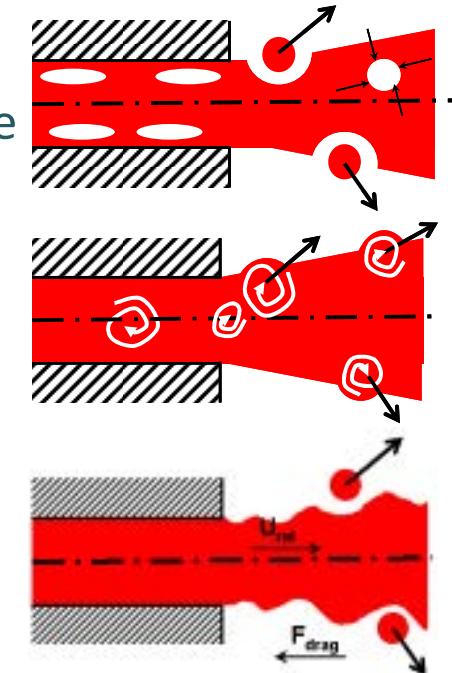
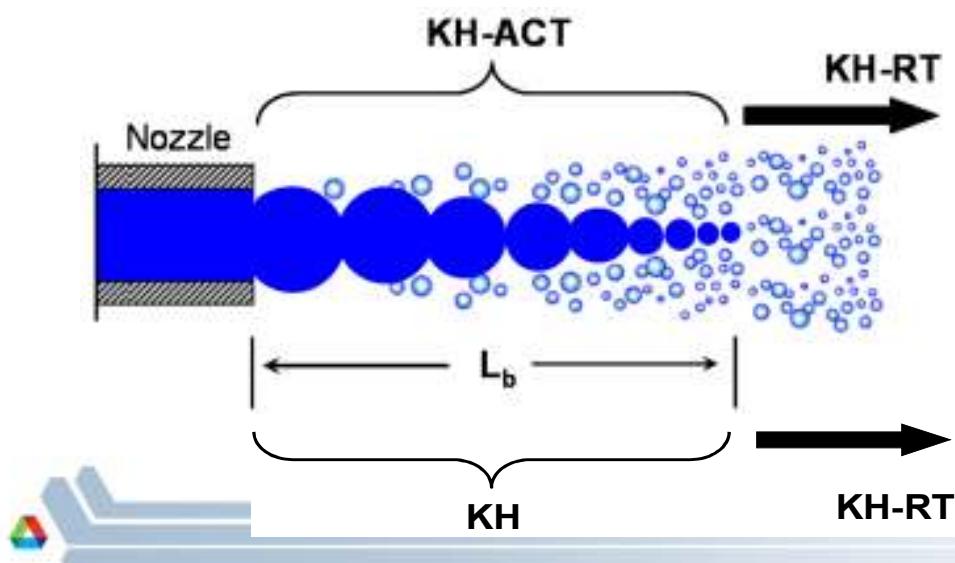
- ❑ Detailed inner-nozzle flow modeling with realistic fuel properties
- ❑ **KH-ACT** primary breakup model:  
Aerodynamics, Cavitation, Turbulence
- ❑ Spray Validation  
X-ray radiography data
- ❑ **Detailed Chemistry:**  
Methyl Butanoate      }  
Methyl Decanoate      } **Biodiesel Surrogate**
- ❑ Validation against **flame lift-off** data



# Primary Breakup Model

## KH-ACT (Kelvin-Helmholtz-Aerodynamics Cavitation Turbulence) Model\* "

- Length and time scales are calculated:
  - Cavitation induced breakup: Based on bubble collapse and burst times
  - Turbulence induced breakup : Based on k- $\epsilon$  model
  - Aerodynamically induced breakup: Based on Kelvin-Helmholtz (KH) and Rayleigh Taylor (RT) instability
- Dominant ratio of length/time scale causes breakup
- Extensive model validation against x-ray data at Argonne



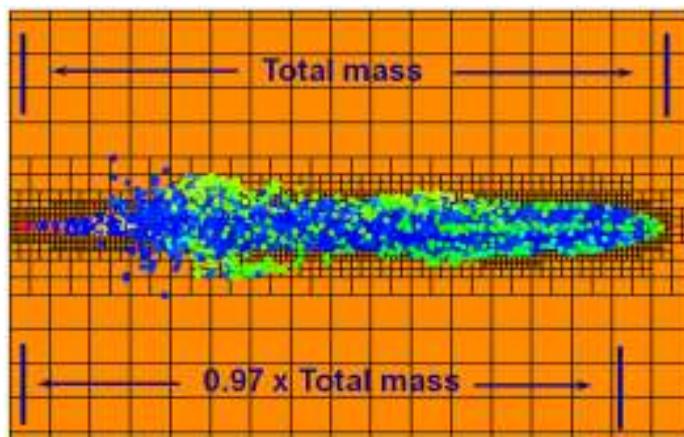
\*Som et al., SAE 2009-01-0838  
Som and Aggarwal, Combustion and Flame 2010

# Modeling Set-up in CONVERGE

- ❑ Liquid Injection using Blob model
- ❑ KH-RT model for secondary breakup
- ❑ Collision and coalescence model
- ❑ Multi-component Evaporation model
- ❑ Dynamic drag model on droplet
- ❑ Turbulent dispersion model
- ❑ Reynolds Average Navier-stokes turbulence model
- ❑ Detailed Chemistry Approach
- ❑ NOx and soot oxidation models

**KH-ACT model implemented "in CONVERGE"**

CONVERGE Manual  
Senecal et al., SAE 2007-01-0159  
S. Som, PhD thesis, UIC 2009

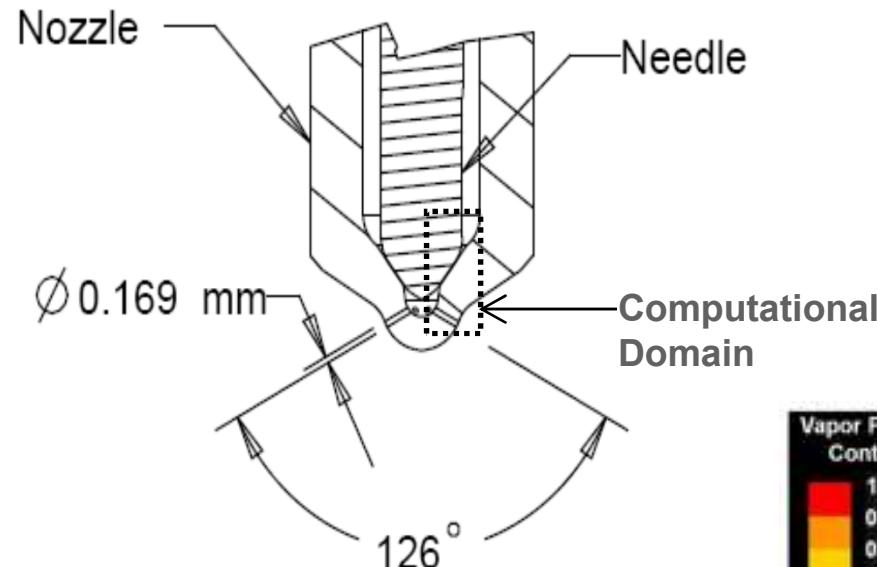


	RANS
Base grid size (mm)	4
Fixed embedding	3
AMR – Velocity field	3
AMR – Temperature field	3
Minimum grid size (mm)	0.25-0.5

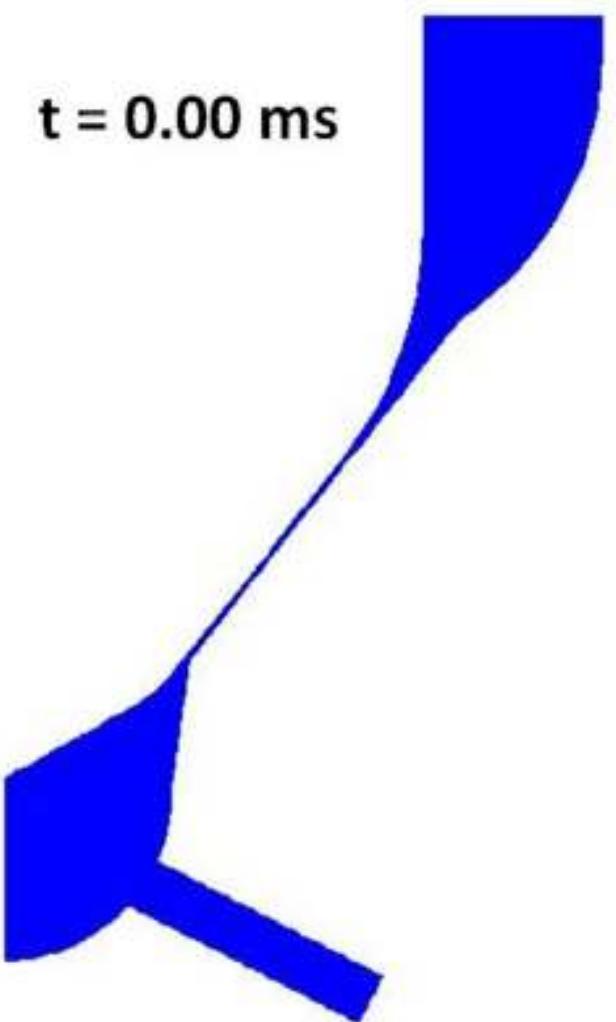
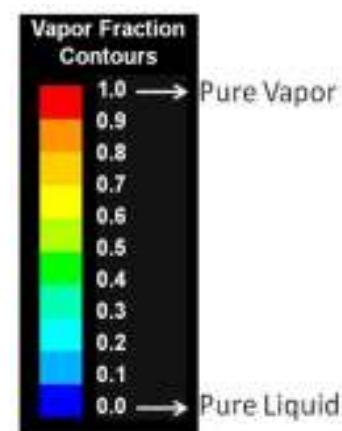
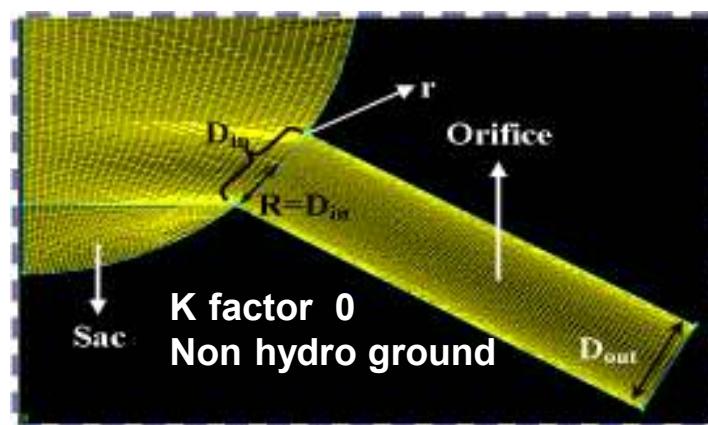


# Injector Geometry and Grid Generated

## 6-hole production Injector



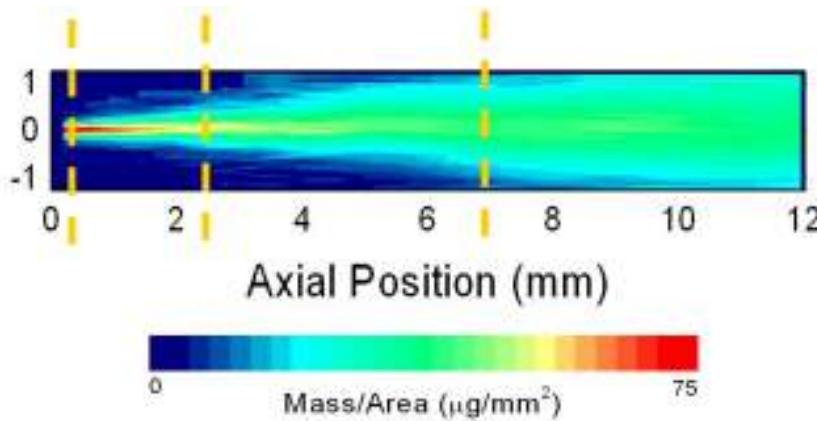
## Nozzle Orifice



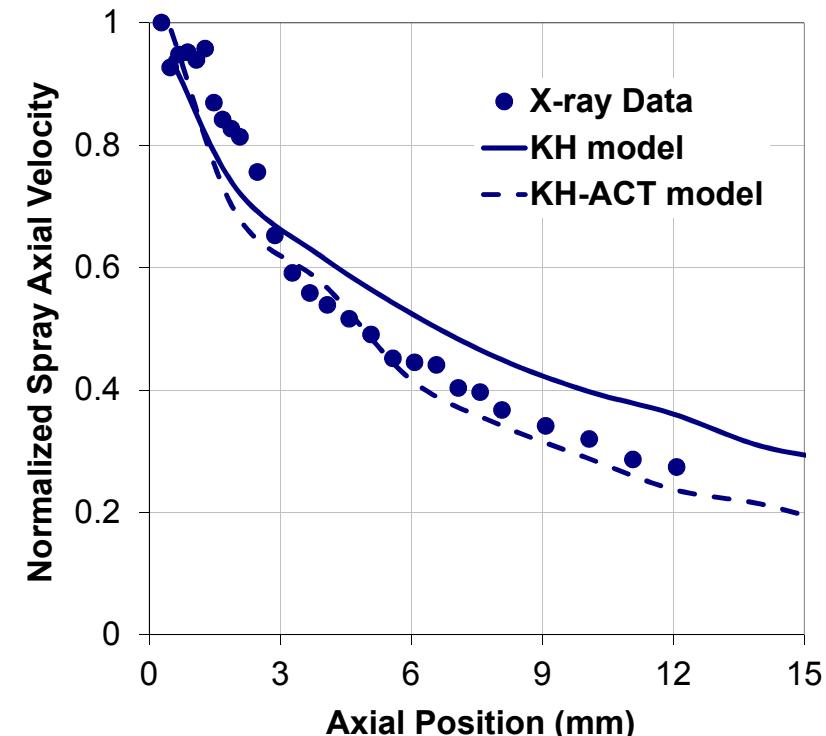
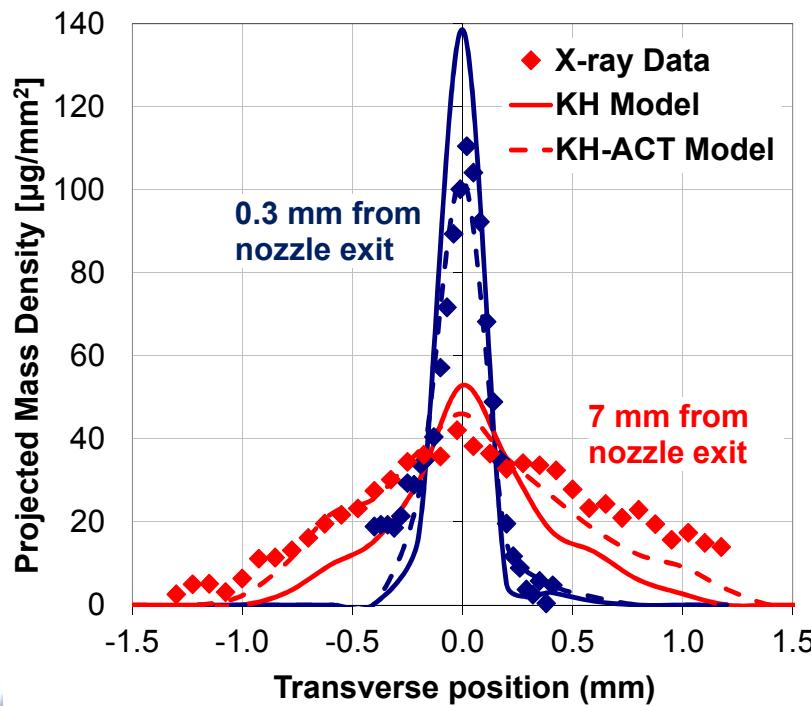
$D=169\mu\text{m}$   
Cylindrical  
Non-hydroground  
 $L/D=4.2$

\*Som et al., FUEL (2010)  
Som et al., JEGTP (2010)

# Spray Validation against X-ray Data



X-ray radiography Data: Ramirez et al., JEF 2009

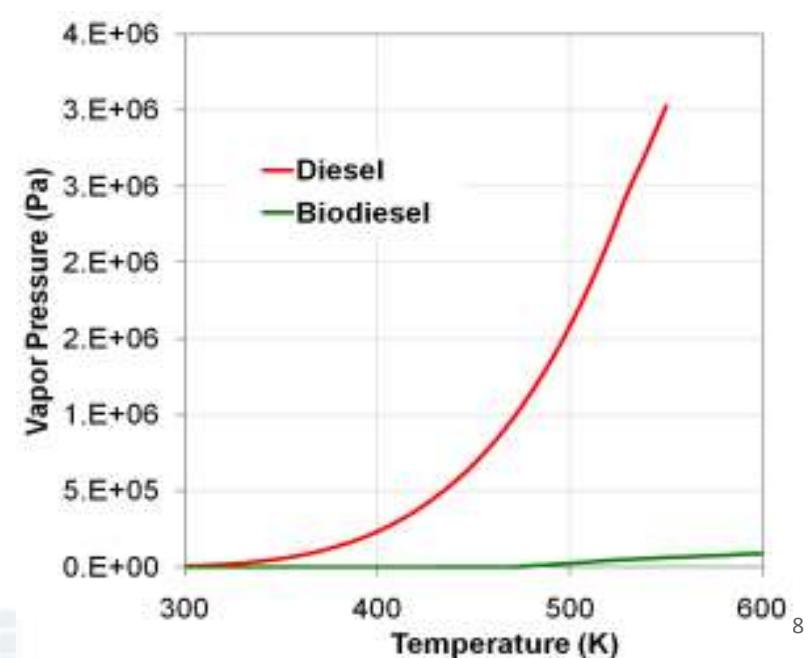
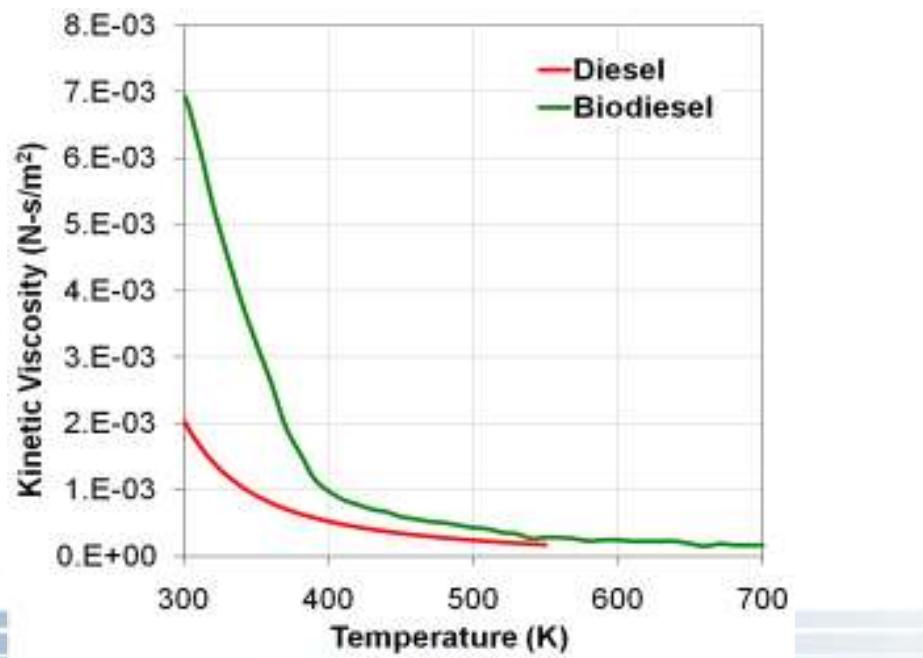


- The spray loses half of its initial velocity within the first 6 mm
- Simulation capture the Gaussian mass distributions from x-ray data well
- Spray Dispersion accurately captured by only the KH-ACT model. KH model under-predicts spray spreading

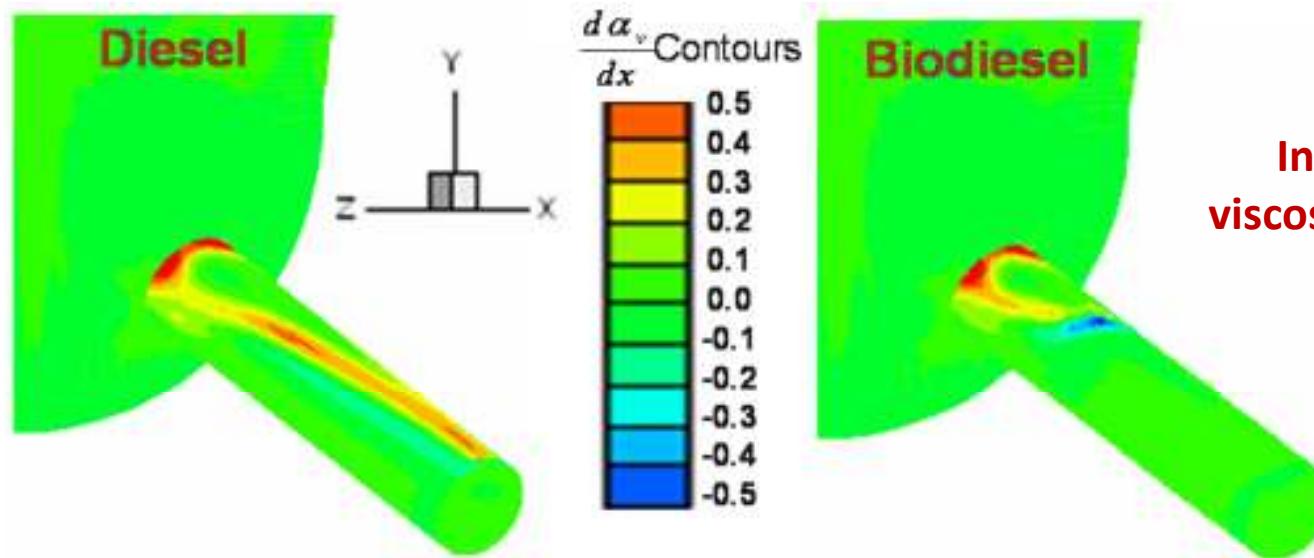
# Differences in Fuel Properties\*

Fuel Property	Diesel	Biodiesel (SME)
Carbon Content [wt %]	87	76.74
Hydrogen Content [wt %]	13	12.01
Oxygen Content [wt %]	0	11.25
Density @ 15°C (kg/m3)	820	877.2
Surface Tension @ 25°C (N/m)	0.020	0.0296
Heat of Combustion (MJ/Kg)	42.0	37.4
Heat of Vaporization (KJ/Kg)	361.0	336.0

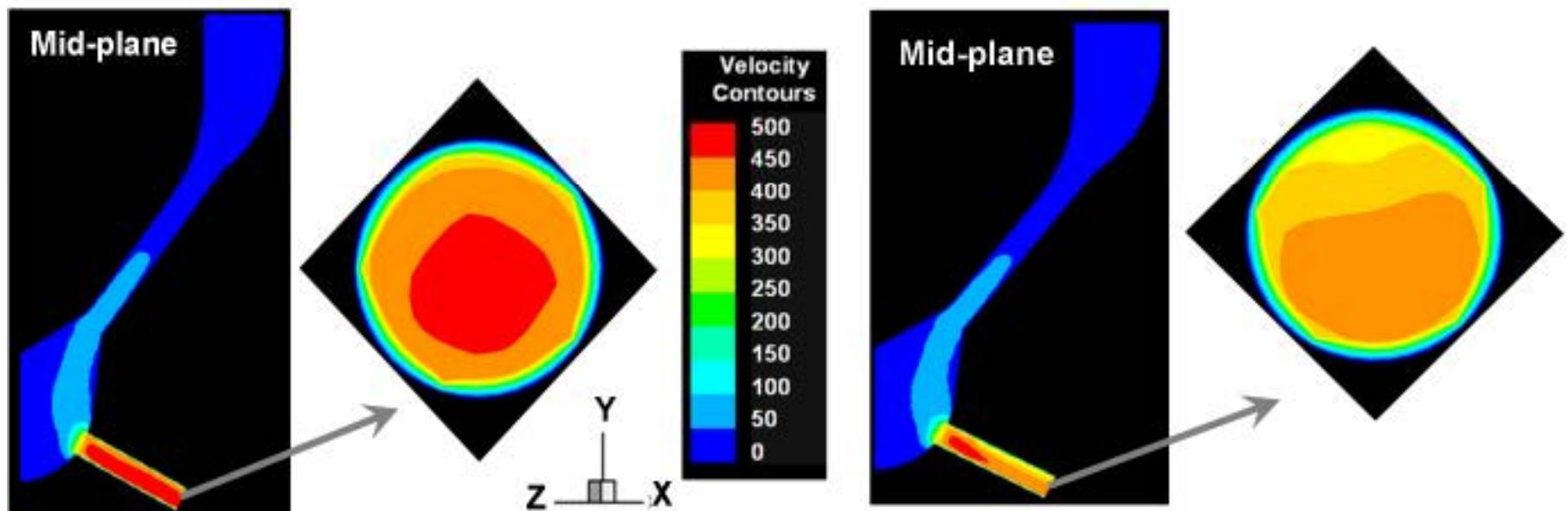
\*S. Som et al., FUEL 2010 "



# Vapor Volume Fraction & Velocity Distribution

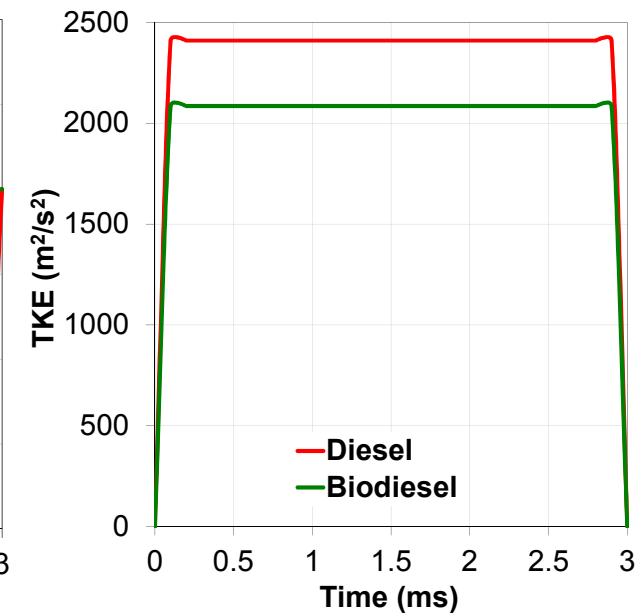
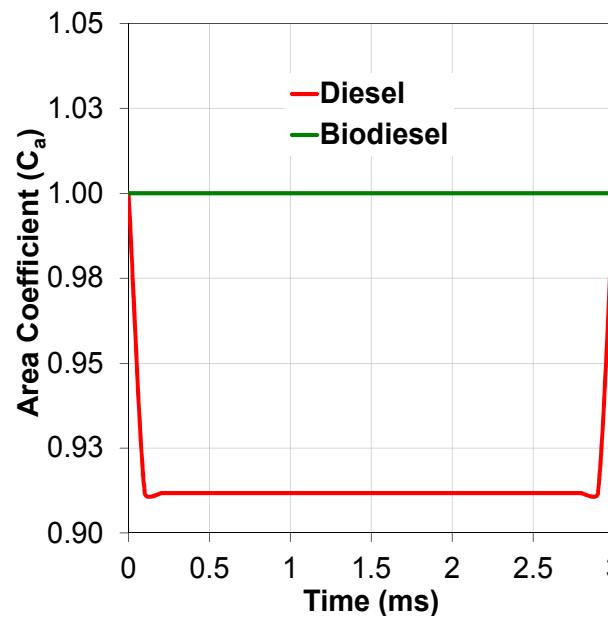
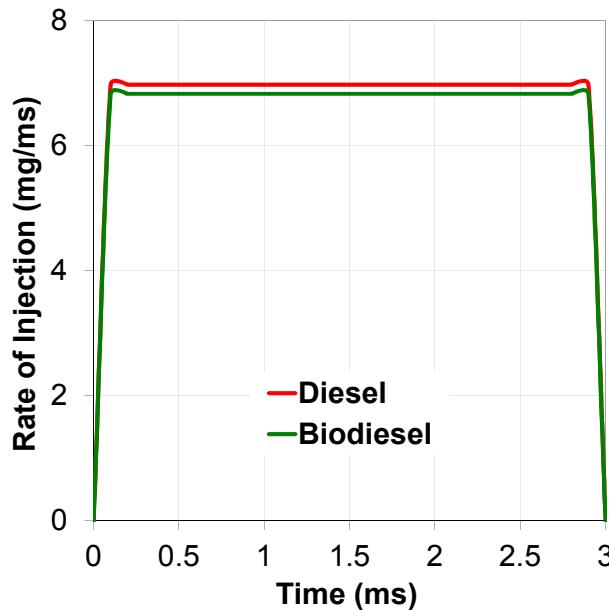


Influenced by density,  
viscosity, and vapor pressure



# Quasi Dynamic Coupling Strategy\*

## Boundary condition for KH-ACT model

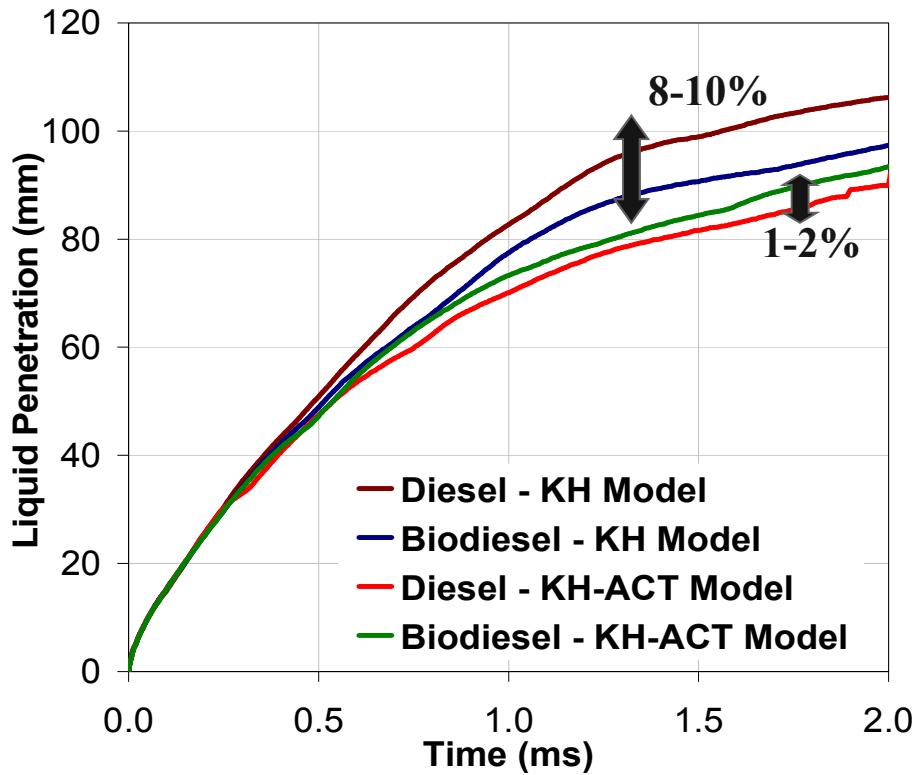


- 1) S Som et al. SAE 2009-01-0838
- 2) Ramirez et al. JEF 2009
- 3) Som and Aggarwal,  
Combustion and Flame 2010

Property	Diesel	Biodiesel
Injection Pressure (bar)	1100   1300	1100   1300
Total Mass Injected (mg)	17.54   20.94	17.18   20.50
Discharge Coefficient ( $C_d$ )	0.64   0.64	0.61   0.62
Area Coefficient ( $C_a$ )	0.92   0.92	1   1
TKE ( $\text{m}^2/\text{s}^2$ )	1409   2410	1356   2135
Injection Duration (ms)	3	3
Ambient Density ( $\text{Kg}/\text{m}^3$ )	34	34
Ambient Temperature (K)	300	300

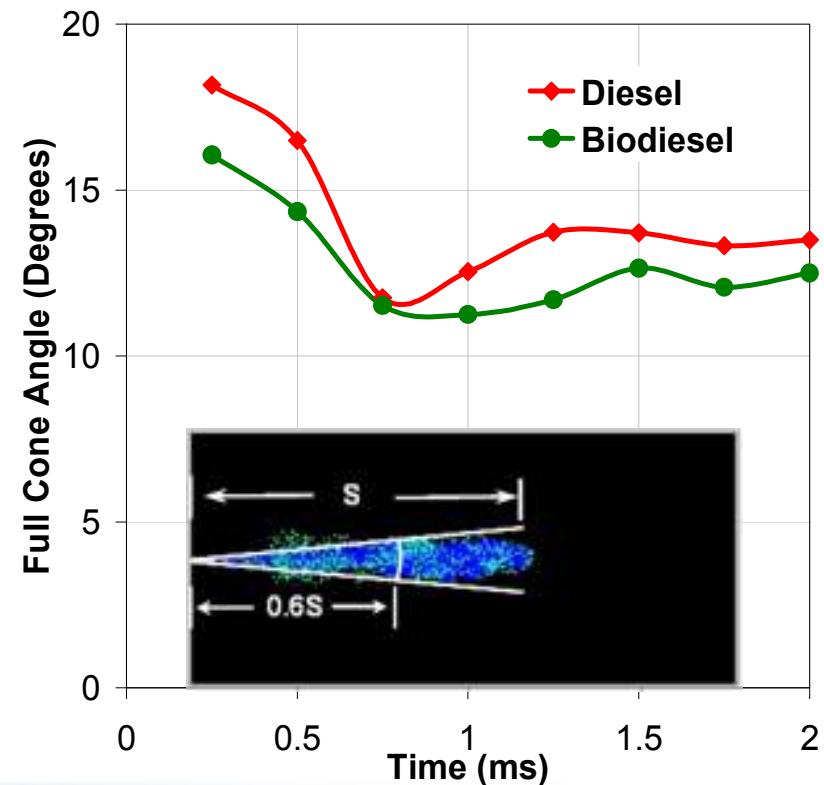


# Spray Penetration & Cone-angle



- ☐ Spray dispersion is lower for biodiesel in the far field region
- ☐ Poorer atomization characteristics for biodiesel due to its higher viscosity, surface tension, lower cavitation and turbulence

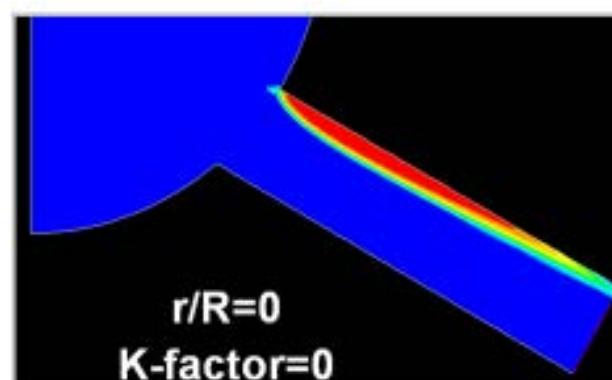
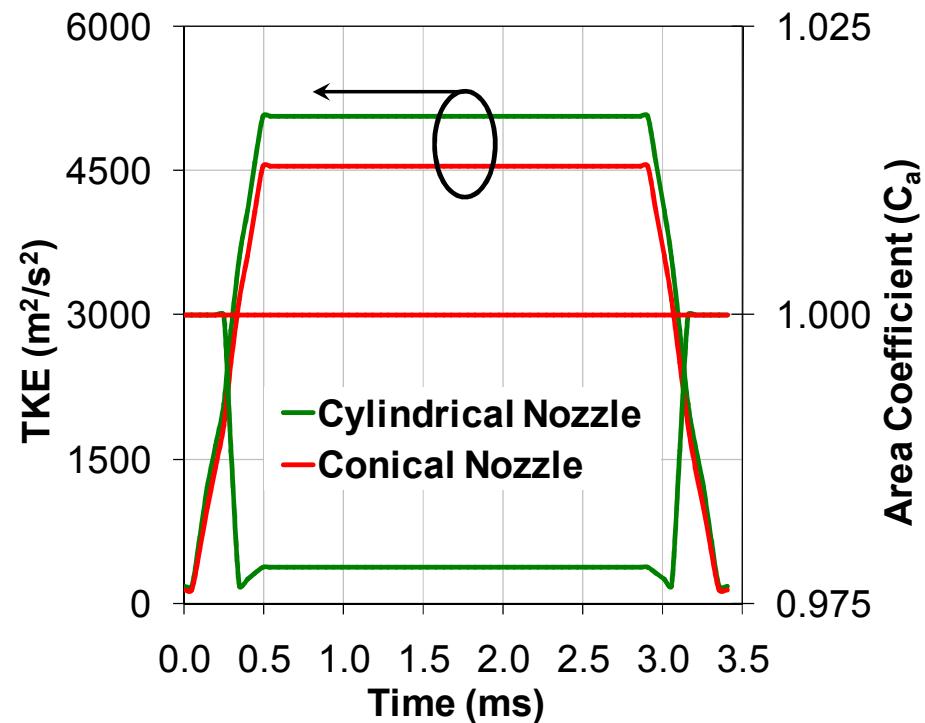
- ☐ Experimental trend: Biodiesel penetrates more than diesel
- ☐ KH-ACT model accurately captures the experimental trend i.e., biodiesel penetrates marginally more than Diesel



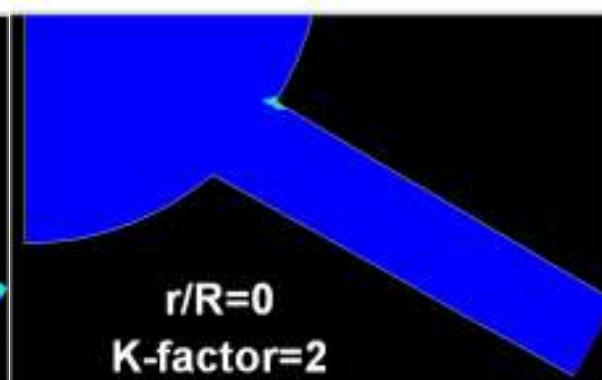
# Effect of Conicity on Inner Nozzle Flow

Geometrical Characteristics	Cylindrical Nozzle	Conical Nozzle
$D_{in}$ ( $\mu\text{m}$ )	169	169
$D_{out}$ ( $\mu\text{m}$ )	169	149
$K_{factor}$	0	2
$L/D$	4.2	4.7

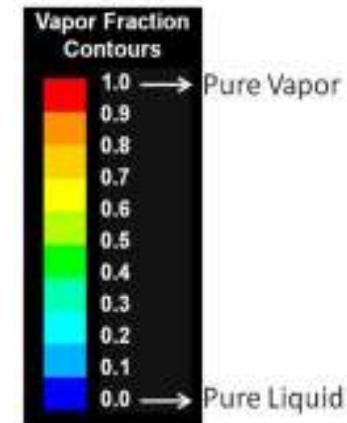
$$K_{factor} = \left( \frac{D_{in} - D_{out}}{10} \right) \mu\text{m}$$



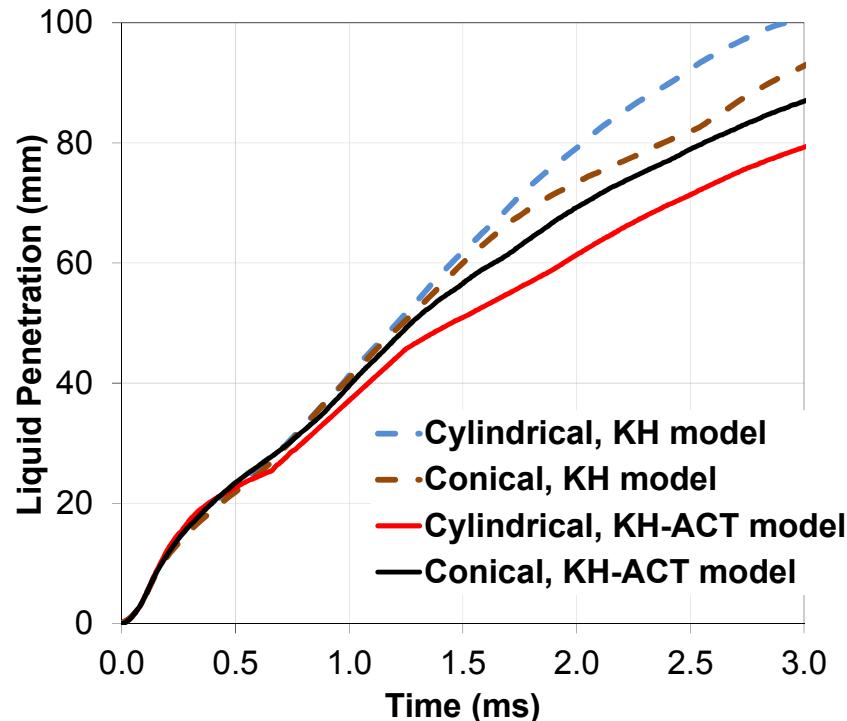
Cylindrical Nozzle



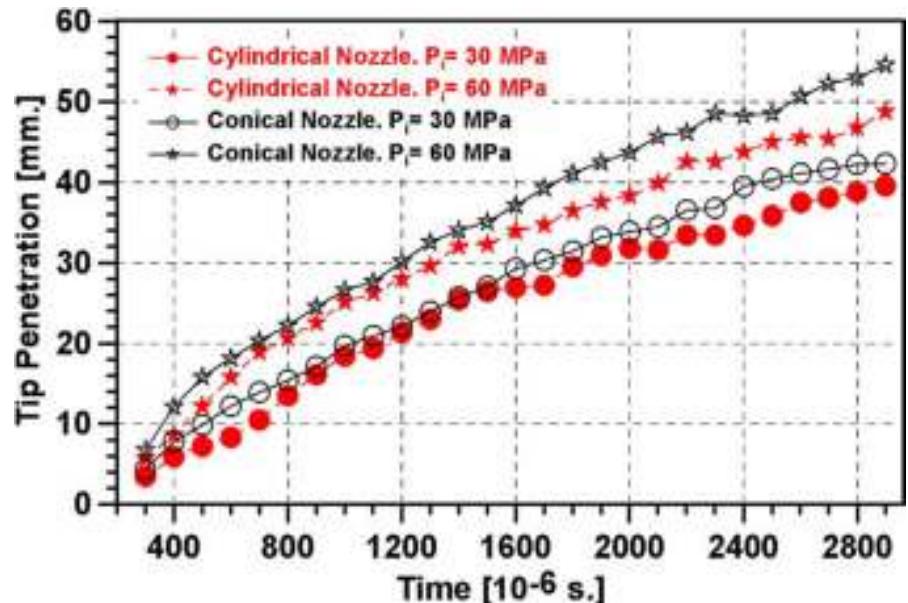
Conical Nozzle



# Influence of Nozzle Geometry on Spray Penetration



F Payri, V Bermudez, R Payri, FJ Salvador: FUEL (2004)

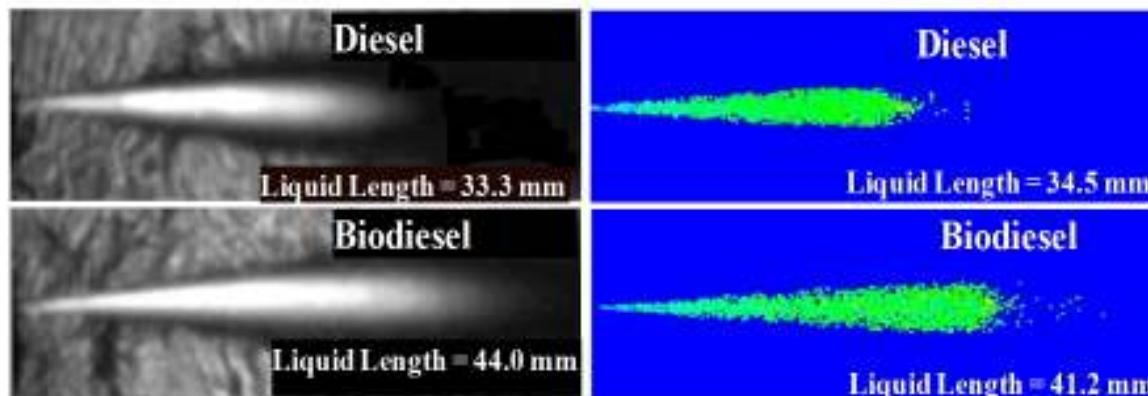


- Penetration characteristics of cylindrical and conical nozzles predicted by KH-ACT model (only) are consistent with experimental trends observed by Payri et al.
- Cylindrical nozzle predicts fastest breakup. This is due to enhanced cavitation and turbulence thus: 1) SMD, 2) Spray penetration are lowest

\*S Som, DE Longman, AI Ramirez, SK Aggarwal. FUEL 2011



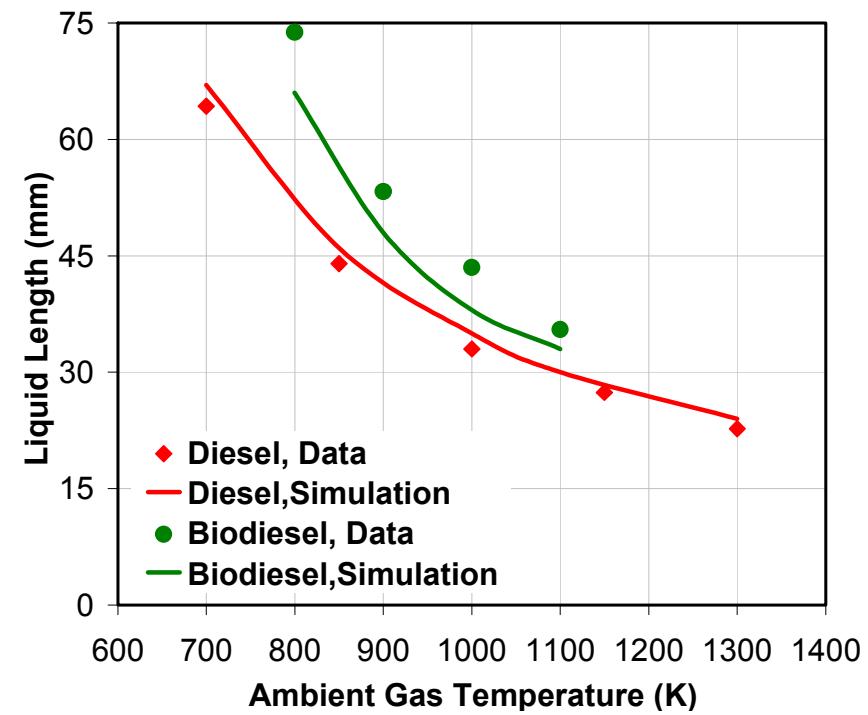
# Evaporating Sprays: Liquid Length



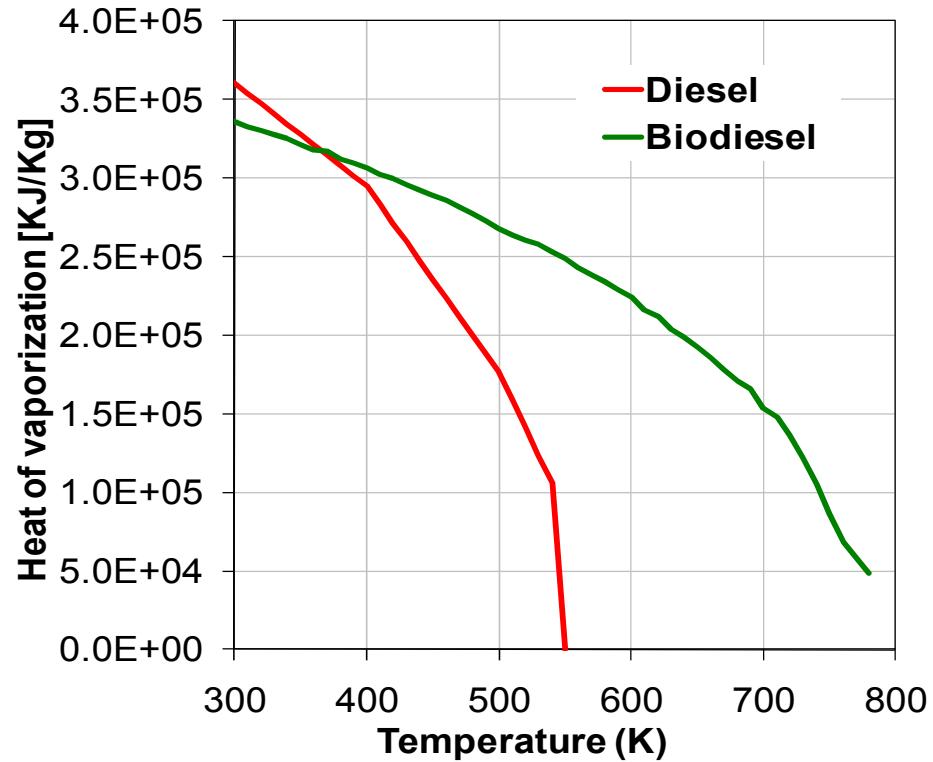
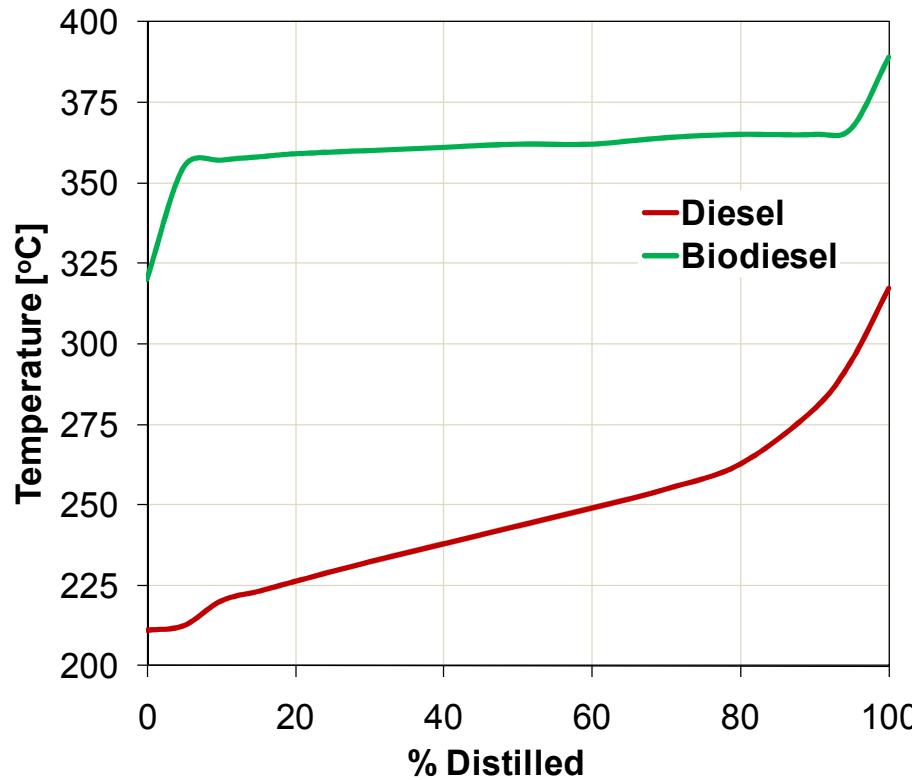
Data from:

- 1) DL Siebers: SAE 980809
- 2) BS Higgins, CJ Mueller, DL Siebers: SAE 1999-01-0519

Injection System	Detroit Diesel, Common Rail
Number of Orifices	1-Cylindrical and Non-hydroground
Orifice Diameter [ $\mu\text{m}$ ]	100 to 500 L/D = 4.2
Injection Pressure [MPa]	40 to 180
Ambient Temperature [K]	700 to 1300
Ambient Gas Composition	$\text{N}_2, \text{H}_2\text{O}, \text{O}_2, \text{CO}_2$
Ambient Density [ $\text{kg}/\text{m}^3$ ]	3.3 to 60
Oxygen concentration	15-21 %
Fuel Density [ $\text{kg}/\text{m}^3$ ]	832
Fuel Temperature [K]	400
Discharge Coefficient	0.78 to 0.84



# Why is the liquid length higher for Biodiesel?

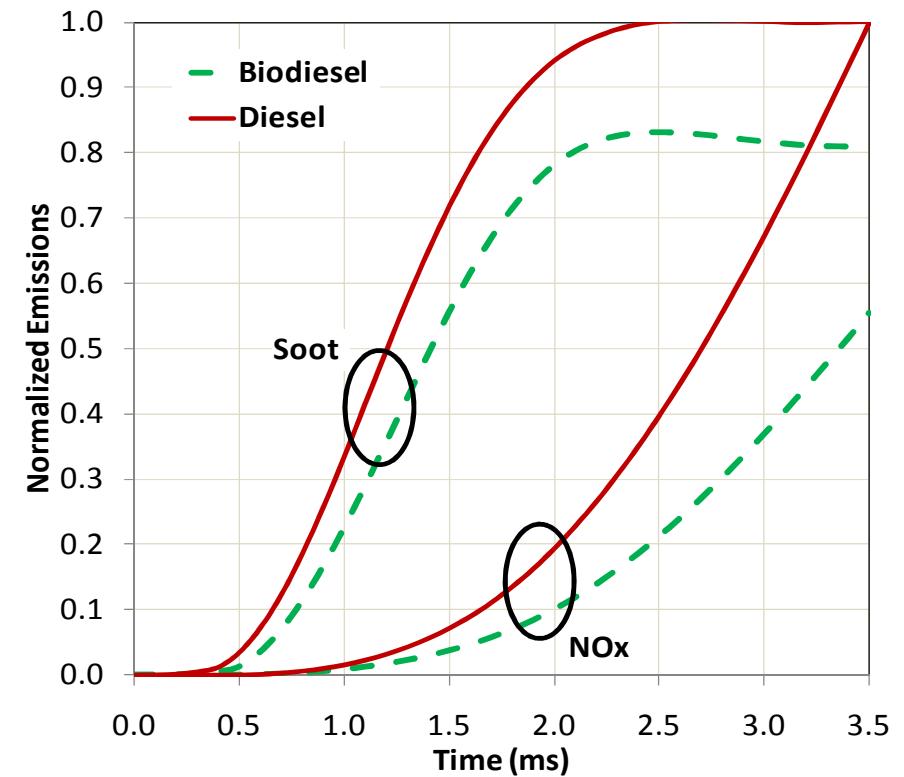
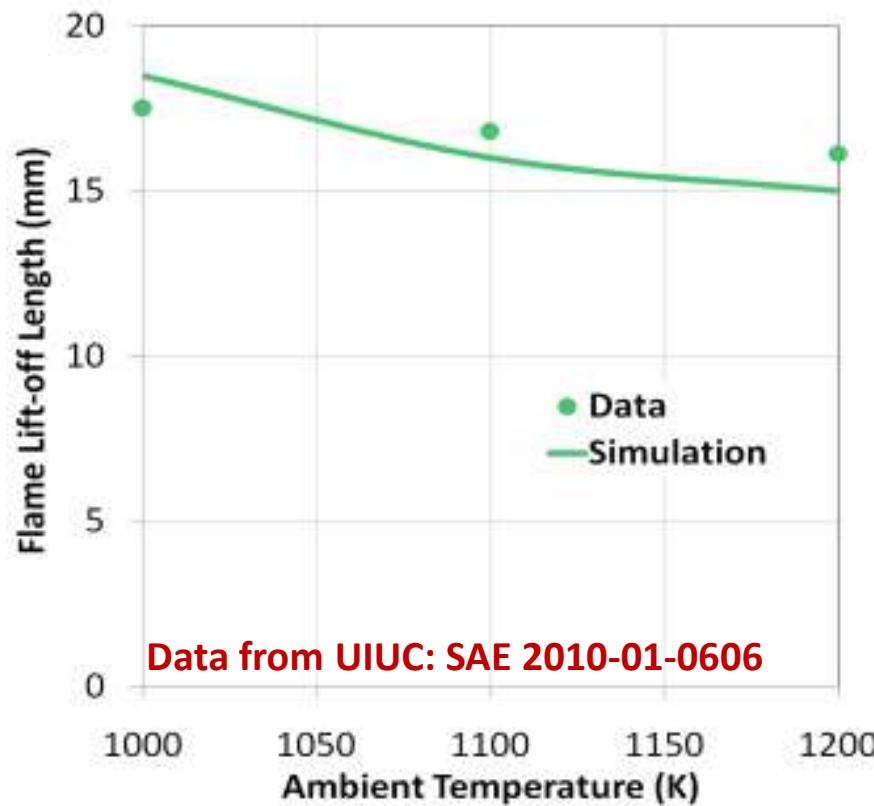


Slower breakup for biodiesel\* is due to lesser amount of inner nozzle turbulence and cavitation. This results in increased spray penetration and reduction in spray cone-angle!

\*S Som, DE Longman, AI Ramirez, SK Aggarwal. *FUEL* 2010



# Combustion Modeling with Detailed Chemistry



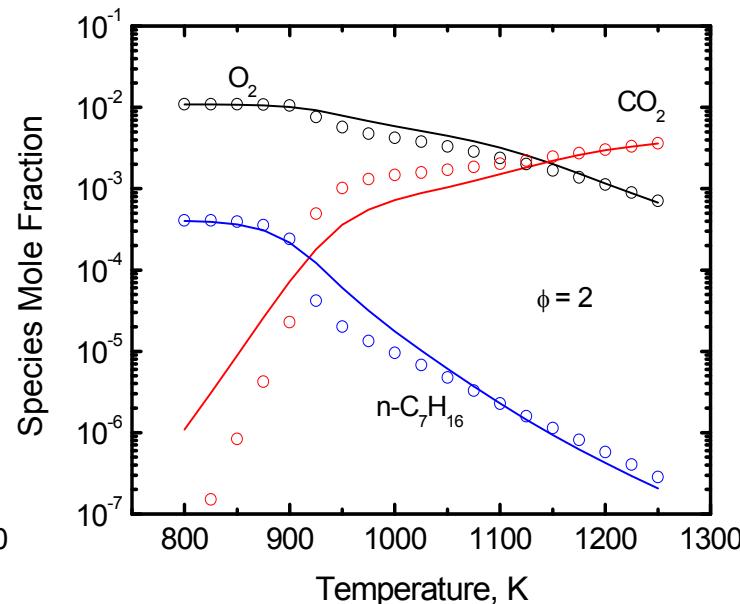
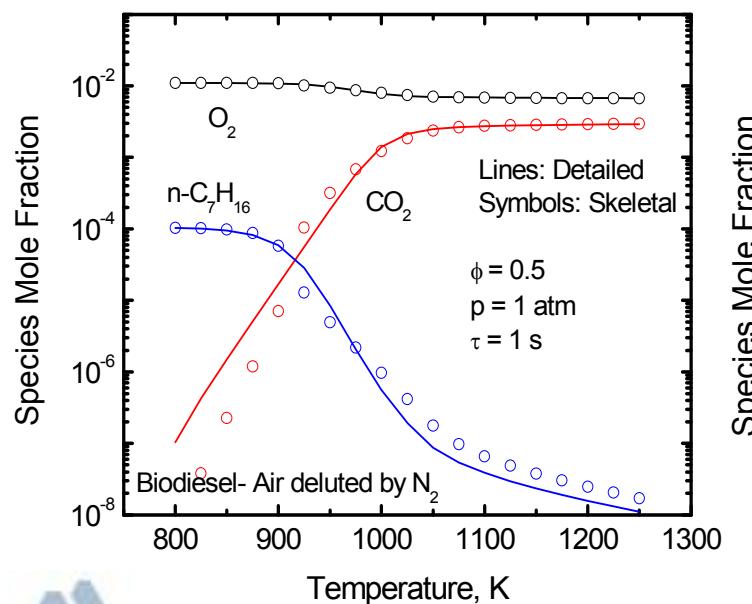
- ❑ Diesel surrogate (n-heptane): 42 species, 168 reaction mechanism from Chalmers University
- ❑ Biodiesel surrogate (methyl butanoate): 41 species, 150 reaction mechanism {Brakora et al. SAE 2008-01-1378}
- ❑ Lower soot emission trends with biodiesel well captured
- ❑ Biodiesel surrogate not able to capture the accurate NOx trends!

# Biodiesel Kinetic Model\* for ICE Applications

- Detailed Mechanism (Methyl Decanoate + Methyl Decenoate + N-heptane) from LLNL 2010:  
3329 species, 10806 reactions
- Directed Relation Graph (DRG) reduction: 664 species, 2672 reactions
- Isomer lumping : 641 species, 2670 reactions
- Sensitivity analysis aided DRG and error cancellation:
- Range of operation:
  - Pressure: 1-100 atm
  - Equivalence ratio: 0.5-2.0
  - Initial temperature: 700 – 1800 K

123 species, 394 reactions  
89 species, 364 reactions

\*Z. Luo, M. Plomer, T. Lu, S. Som, D.E. Longman, IC#18.  
US National Combustion Institute meeting, March 2011



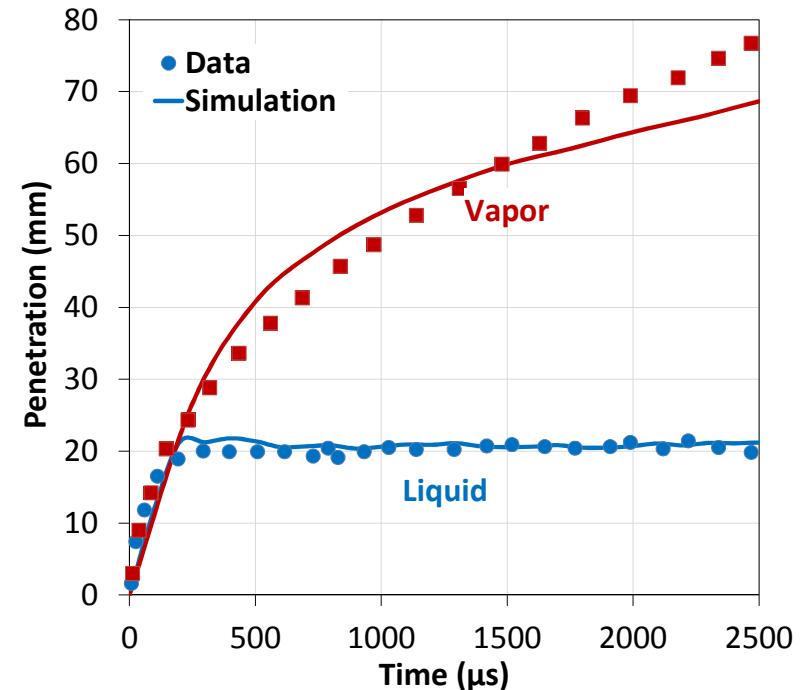
JSR Data:  
Dagaut et al. PCI 31  
(2007)



# Biodiesel: Case set-up

## Injection & Ambient conditions for Biodiesel studies at Sandia\*

Parameter	Quantity
Injection System	Bosch Common Rail
Nozzle Description	Single-hole, mini-sac
Duration of Injection [ms]	7.5
Orifice Diameter [ $\mu\text{m}$ ]	90
Injection Pressure [Bar]	1400
Fill Gas Composition (mole-fraction)	$\text{N}_2=0.7515, \text{O}_2=0.15,$ $\text{CO}_2=0.0622, \text{H}_2\text{O}=0.0363$
Chamber Density [ $\text{kg}/\text{m}^3$ ]	22.8
Chamber Temperature [K]	1000
Fuel Density [ $\text{kg}/\text{m}^3$ ]	877
Fuel Injection Temperature [K]	363



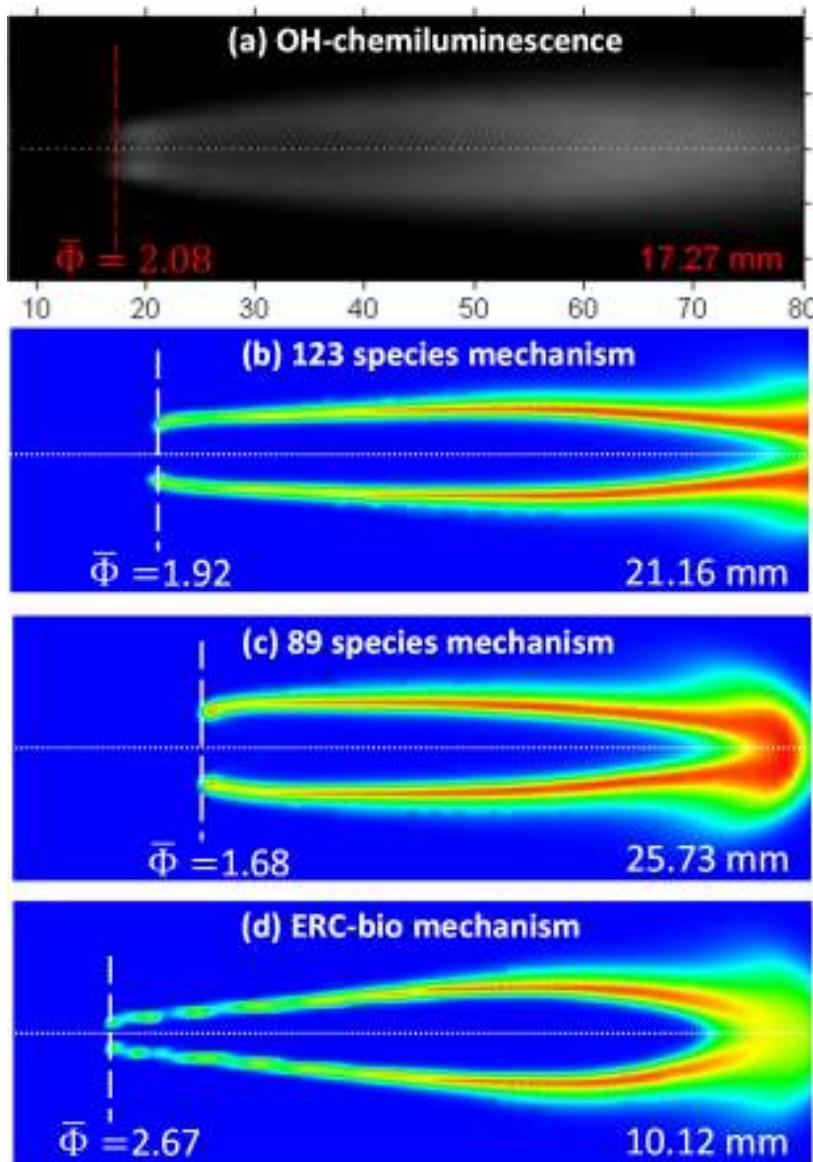
\*Pickett & Co-workers (2011) *Personal Communication*

JG Nerva, CL Genzale, JMG Oliver, LM Pickett. Fundamental Spray and Combustion Measurements of Biodiesel under Diesel steady conditions. *Under preparation*

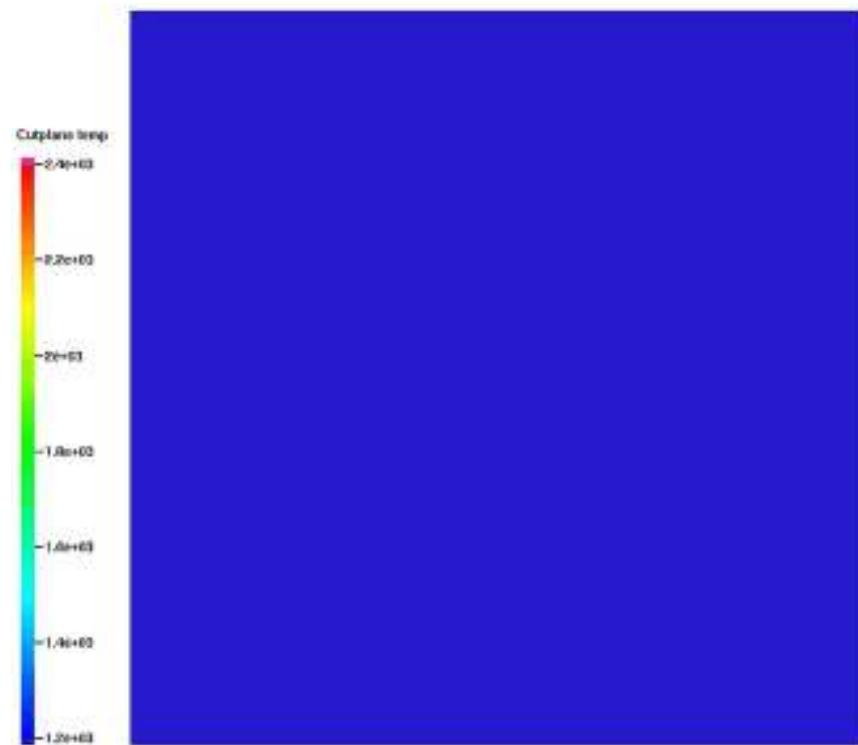
- Lu – 123: 123 species, 394 reactions. Paper # IC18. US National Combustion Meeting, March 2011
- Lu – 89 : 89 species, 364 reactions. Paper # IC18. US National Combustion Meeting, March 2011
- ERC-bio mechanism: 41 species, 150 reactions. SAE Paper No. 2008-01-1378



# Validation of Different Reaction Mechanisms



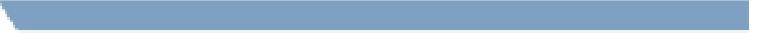
	Ignition Delay (ms)
Sandia Data	0.396
Lu - 123 species	0.510
Lu - 89 species	0.580
ERC-Bio mechanism	0.220



# Summary & Future Work

- ❑ Developed **KH-ACT primary breakup model:**
  - ✓ Captures biodiesel spray characteristics accurately
  - ✓ Predicts influence of nozzle orifice geometry
- ❑ Integrated Modeling Approach:
  - ✓ Coupled nozzle-flow, spray, and combustion modeling
  - ✓ Robust **validation against x-ray radiography data**
- ❑ Combustion modeling with detailed chemistry:
  - ✓ MD+MD9D+NHPT as a surrogate for biodiesel
  - ✓ **123 species (MD+MD9D+NHPT) mechanism** captures flame characteristics well
- ❑ Full-cycle engine simulations with KH-ACT model against CAT single-cylinder engine data
  - Engine testing currently in progress at Argonne
- ❑ Turbulence Modeling:
  - Coupling **high-fidelity LES model** with detailed chemistry



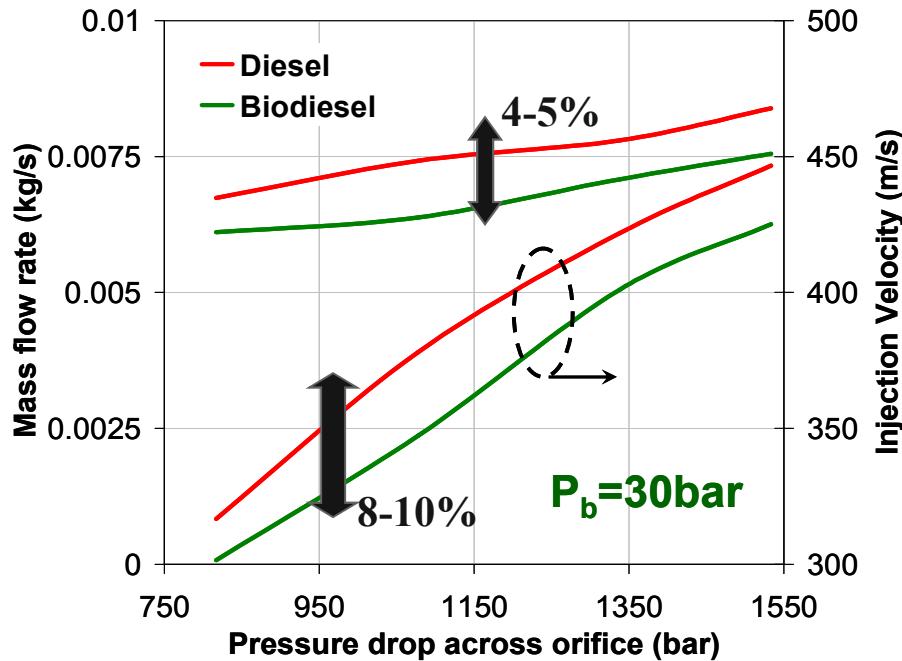


# Thank You

Contact: [ssom@anl.gov](mailto:ssom@anl.gov) [dlongman@anl.gov](mailto:dlongman@anl.gov)

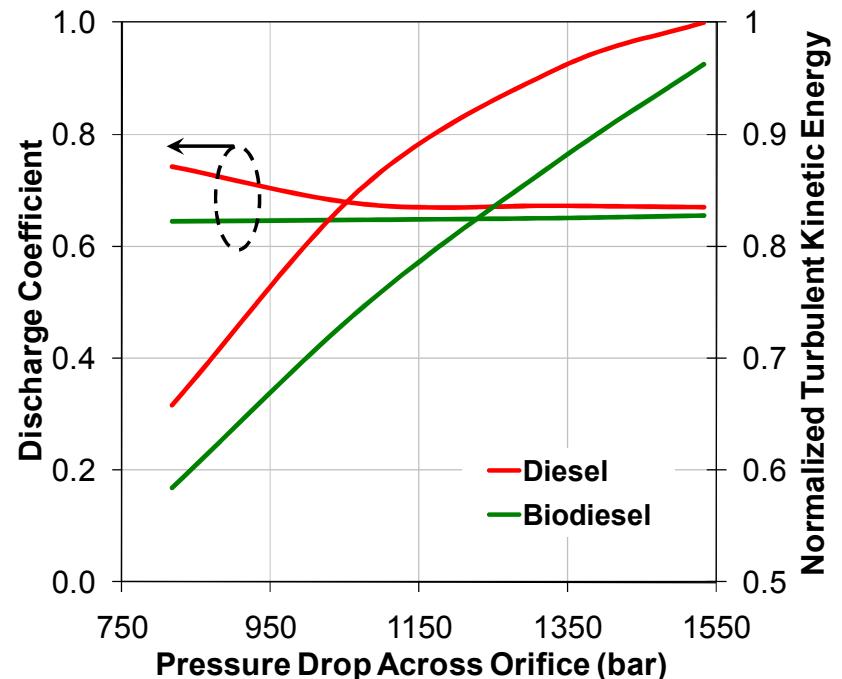


# Nozzle Exit Characteristics



- ❑ Lower levels of turbulence and cavitation for biodiesel
- ❑ Breakup process with biodiesel may be slower!

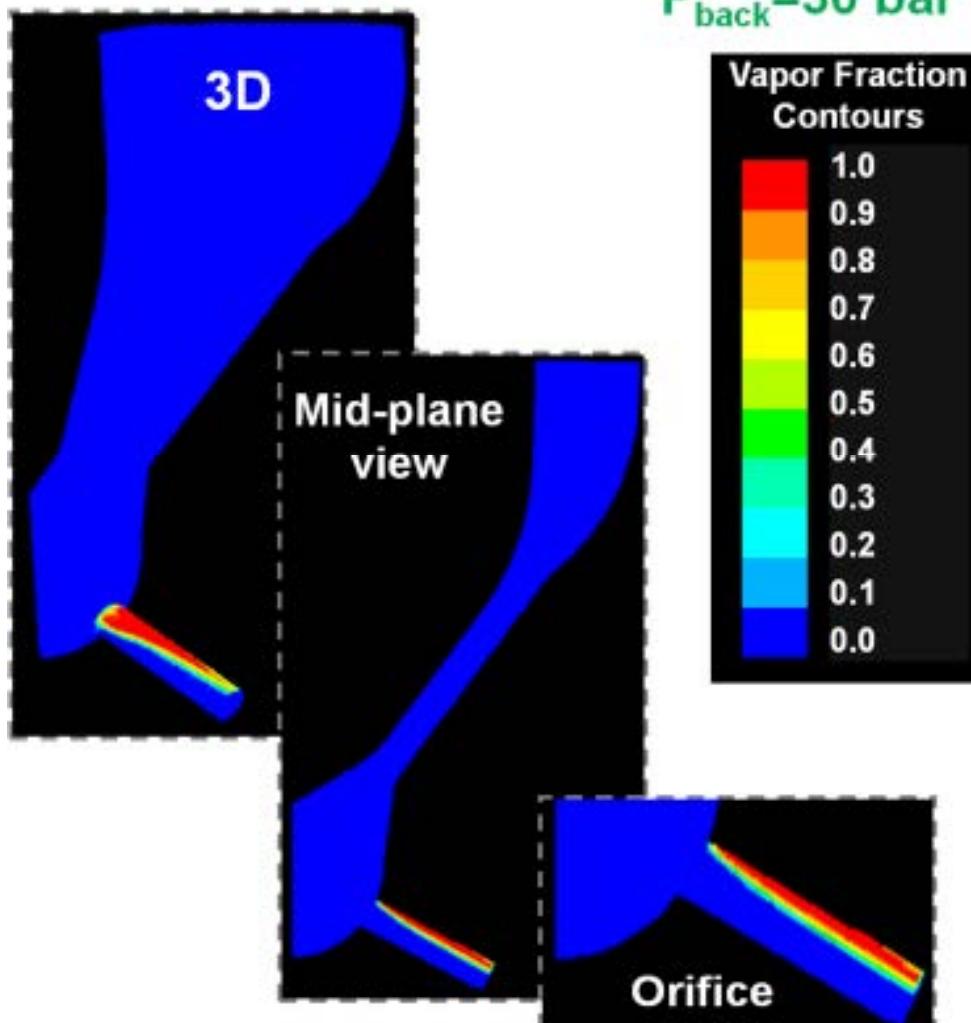
$$C_d = \frac{\dot{M}_{actual}}{\dot{M}_{th}} = \frac{\dot{M}_{actual}}{A_{th} \sqrt{2 * \rho_f * (P_{inj} - P_{back})}}$$



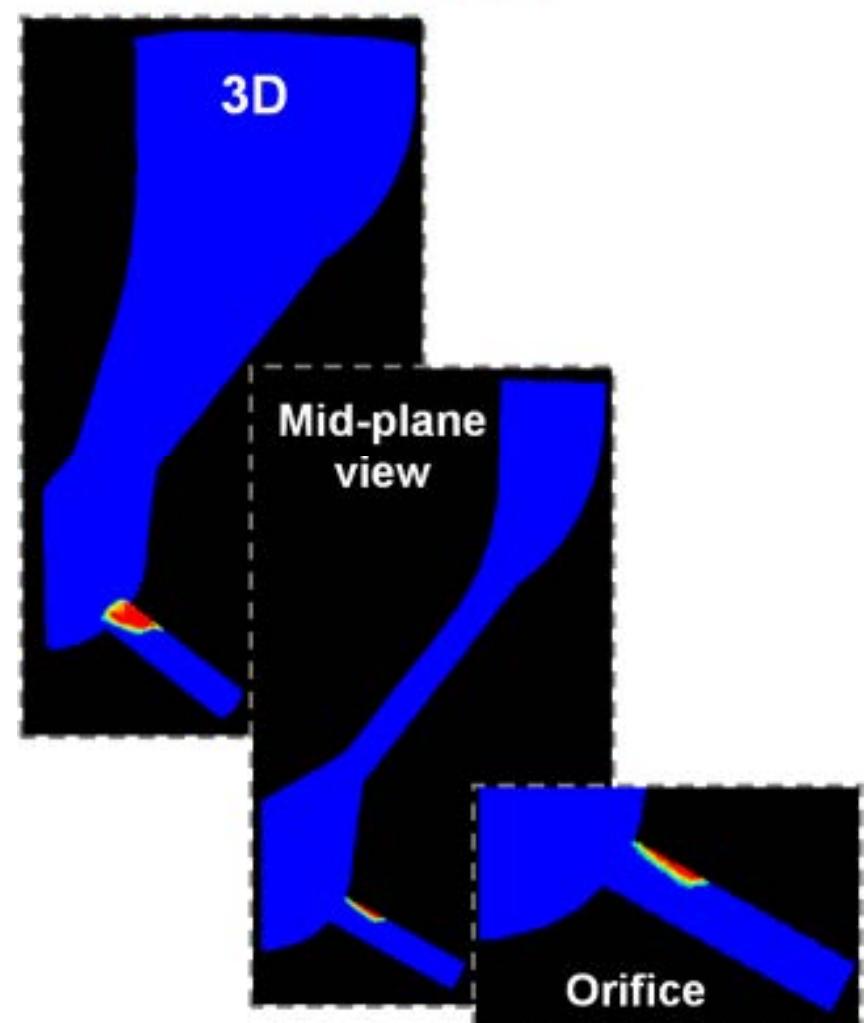
- ❑ Lower injection velocity, mass flow rate, and discharge coefficient for biodiesel
- ❑ This is due to biodiesel's significantly higher molecular and turbulent viscosity
- ❑ Significant differences in inner nozzle flow characteristics

# Vapor Distribution

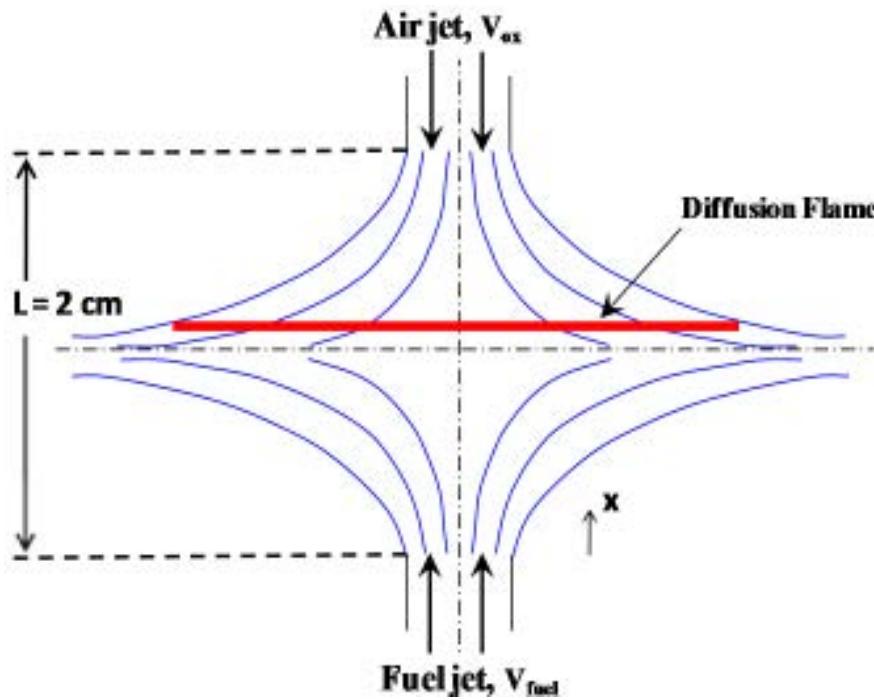
Diesel



Biodiesel

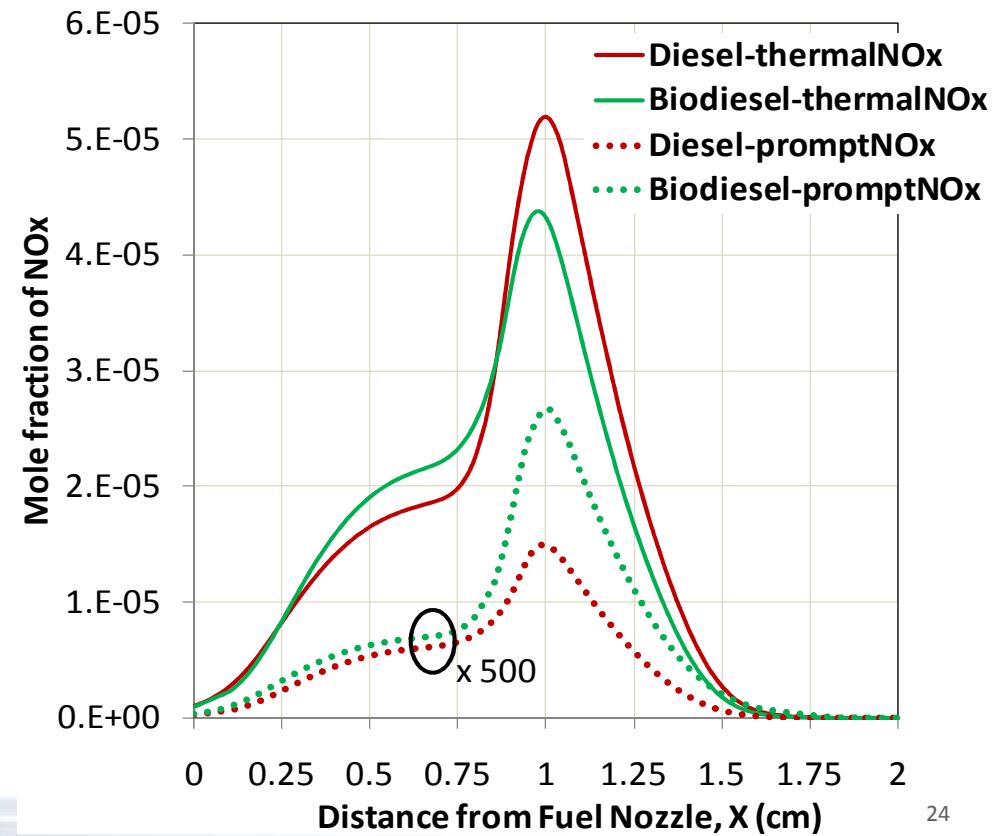


# Emission Characteristics in 1-D Configuration

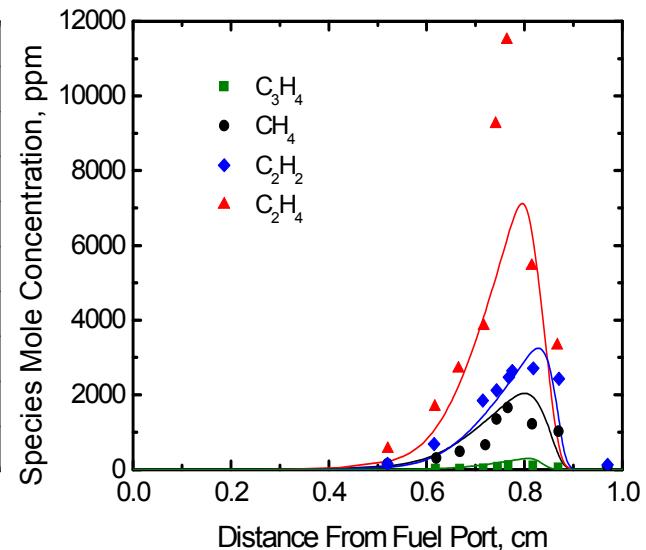
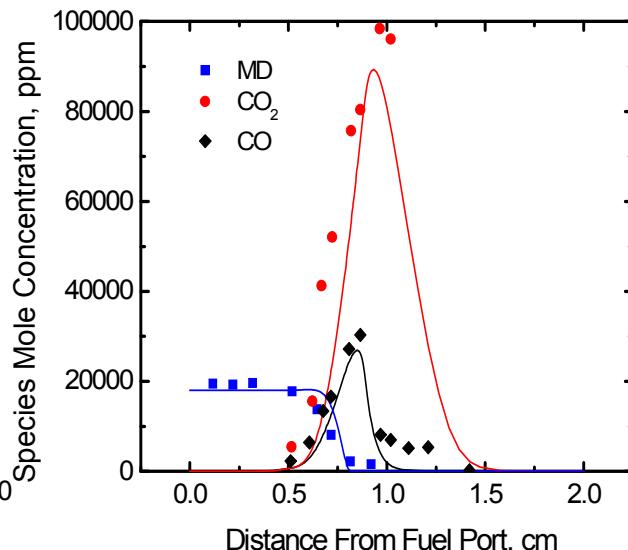
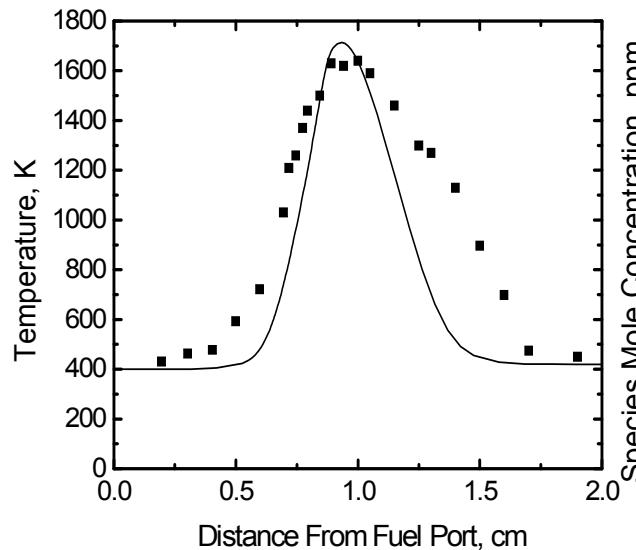


- ❑ Counter-flow configuration to study the NOx chemistry further
- ❑ GRI-3.0 NOx chemistry consisting of prompt, thermal,  $\text{N}_2\text{O}$
- ❑ Simulations performed in CHEMKIN 4

- ❑ Prompt NOx higher for biodiesel compared to diesel
- ❑ Thermal NOx higher for diesel
  - Radical pool not captured properly by the mechanisms



# Biodiesel Kinetic Model\* for High-T Applications

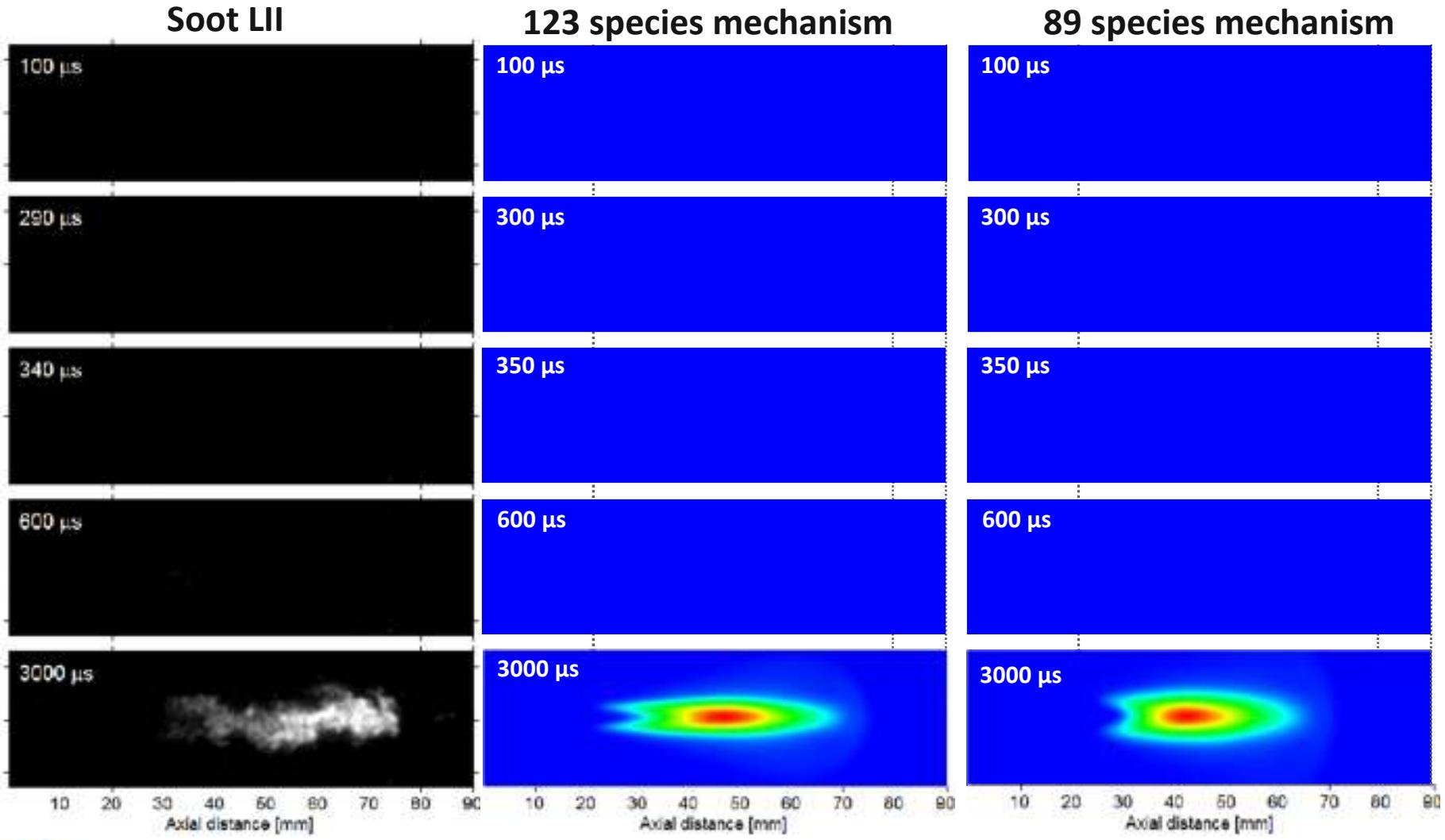


- Detailed Mechanism (Methyl Decanoate + Methyl Decenoate + N-heptane) from LLNL 2010:  
3329 species, 10806 reactions
- Directed Relation Graph (DRG) reduction: 472 species, 2237 reactions
- Isomer lumping and DRG reduction: 242 species, 1819 reactions
- Sensitivity analysis aided DRG: 118 species, 83 reactions final mechanism
- Range of operation:
  - Pressure: 1-100 atm
  - Equivalence ratio: 0.5-2.0
  - Initial temperature > 1000 K

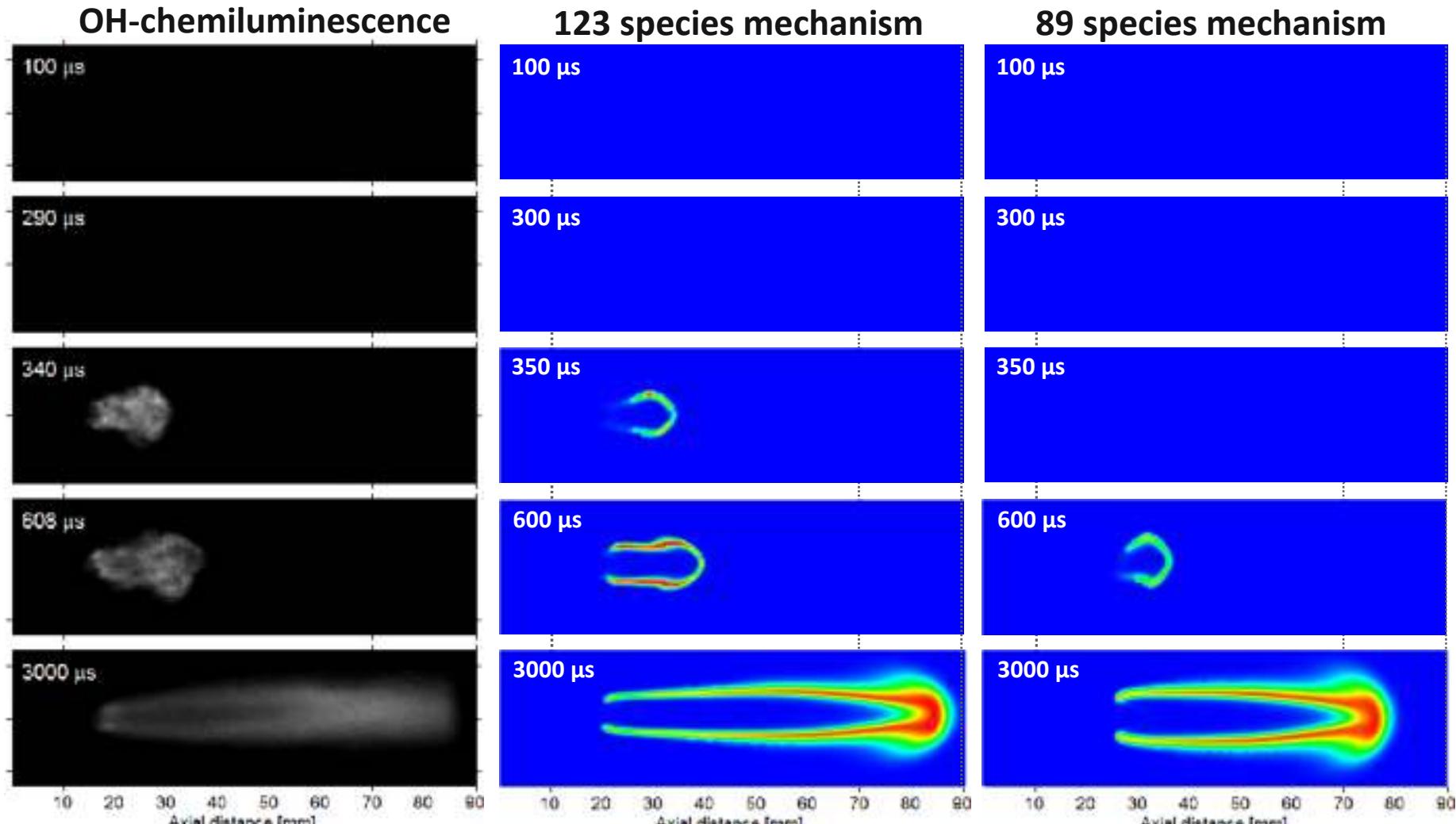
\* Z. Luo, M. Plomer, T. Lu, S. Som, D.E. Longman,  
*Energy & Fuels* (2010)



# Soot Validation with MD+MD9D+NHPT Mechanism



# Further Validation of Biodiesel Kinetic Models



~ 160 hours on 8 processors

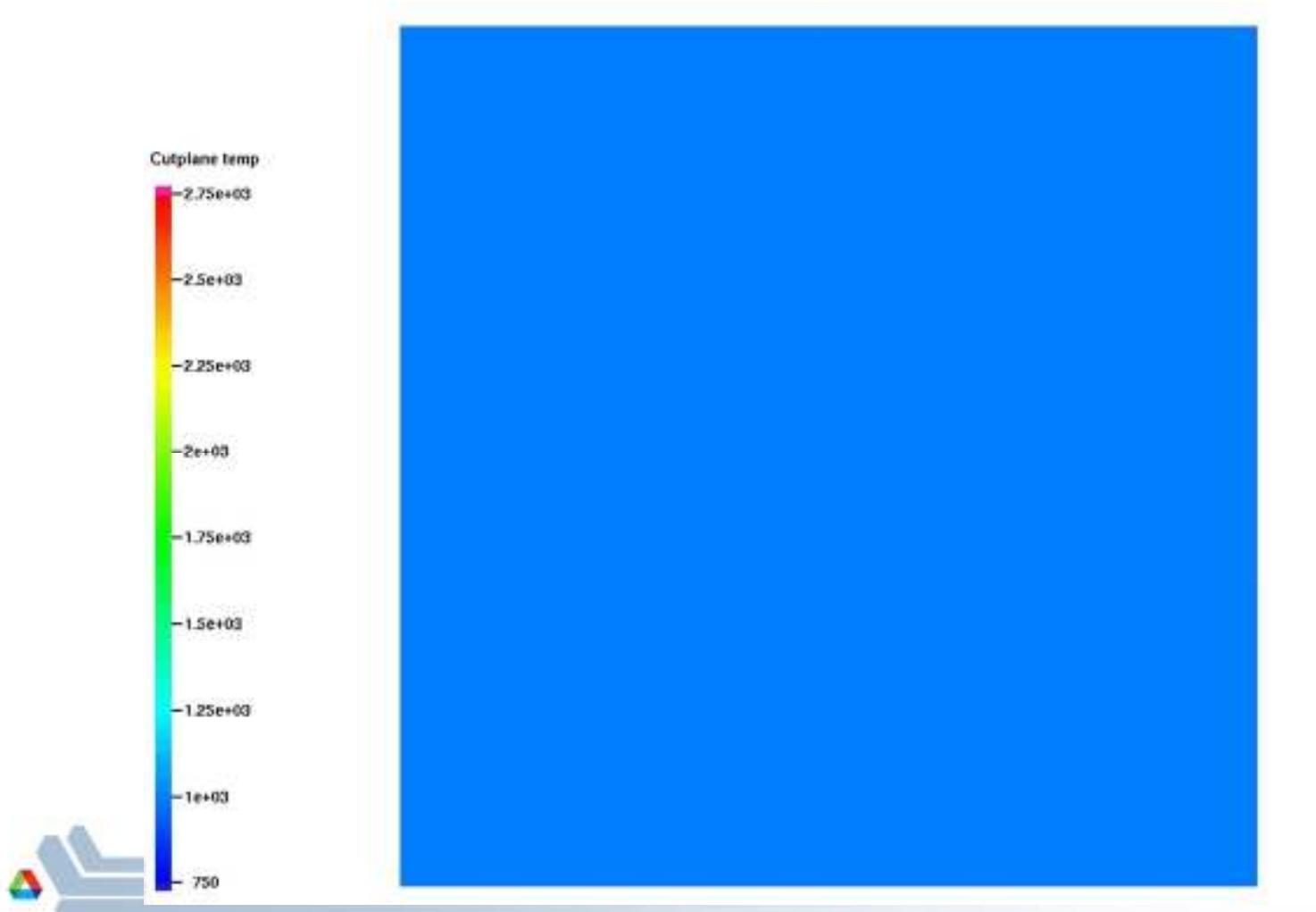
~ 85 hours on 8 processors



# LES Modeling with Detailed Chemistry

Smagorinsky based LES Model:

- 0.125 mm minimum grid size
- 2 millions grid points for resolving a 108 mm (each side) cube
- 8-10 days on 24 processors



# Soot Prediction with RANS & LES Models

